



# The evaluation of spent coffee grounds as feedstock for continuous hydrothermal liquefaction

*13 September*

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# Background and motivation:

- Fossil fuels provides most of the worlds energy <sup>[1]</sup>
- Renewable fuels: Food vs. Fuels
- Spent coffee grounds (SCG) is a good alternative
  - SCG is not a food source
  - Global coffee consumption in 2017 was 9.51 million tons <sup>[2]</sup>
  - SCG is currently being sent to the landfill





# Background and motivation:

- Thermochemical reaction methods:
  - Pyrolysis vs. hydrothermal liquefaction (HTL)
    - Pyrolysis requires intensive drying <sup>[4]</sup>
    - SCG has a high moisture content of 60 wt.% <sup>[5]</sup>
    - SCG is ideally suited for HTL
    - HTL produces a higher quality biocrude <sup>[4]</sup>

# Aims and objectives:

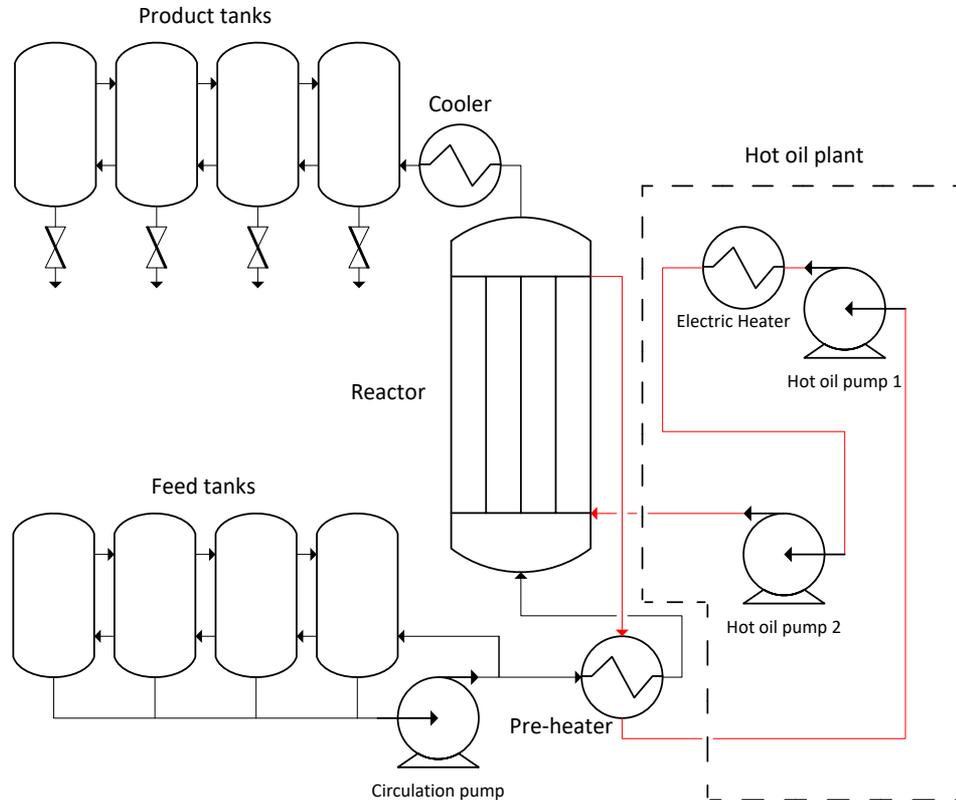
- Aim
  - To determine if SCG could be utilised as a feedstock in a continuous HTL reactor for the production of biocrude and biochar
- Objectives
  - Optimal biomass loading
  - Effect of retention time on product yield and quality



# Reactor setup:



# Reactor setup: PFD



# Experimental procedure: Reactor conditions

Reactor condition	Range	Unit
Hot oil temperature	300 – 305	°C
Pressure	90 – 95	Bar
Flow rate	60 – 120	L/h
Residence time	10 - 20	min



# Results: Fibre Analysis

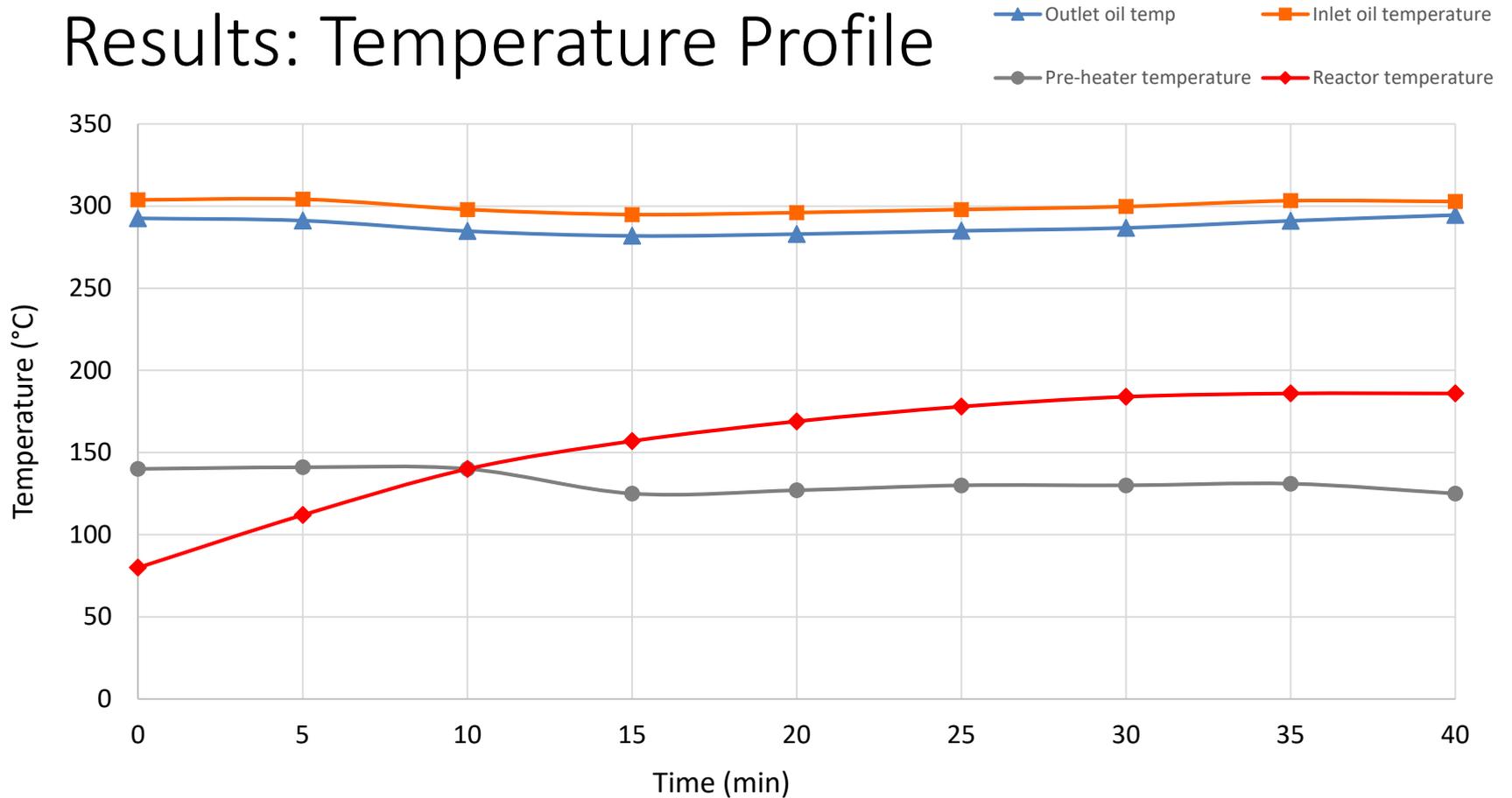
Component	wt. %
Ash	1.34
Protein	12.71
Fat (Ether extraction)	12.86
Carbohydrates	67.62
Hemicellulose	34.97
Cellulose	19.26
Lignin	10.54

# Results: Biomass loading

- The biomass loading was varied:
  - 5 vol.% - 3 vol.%
  - SCG was not pre-treated
- Optimal biomass loading did not cause blockages
- A few blocked reactors later:
  - The optimal biomass loading was 3 vol.%

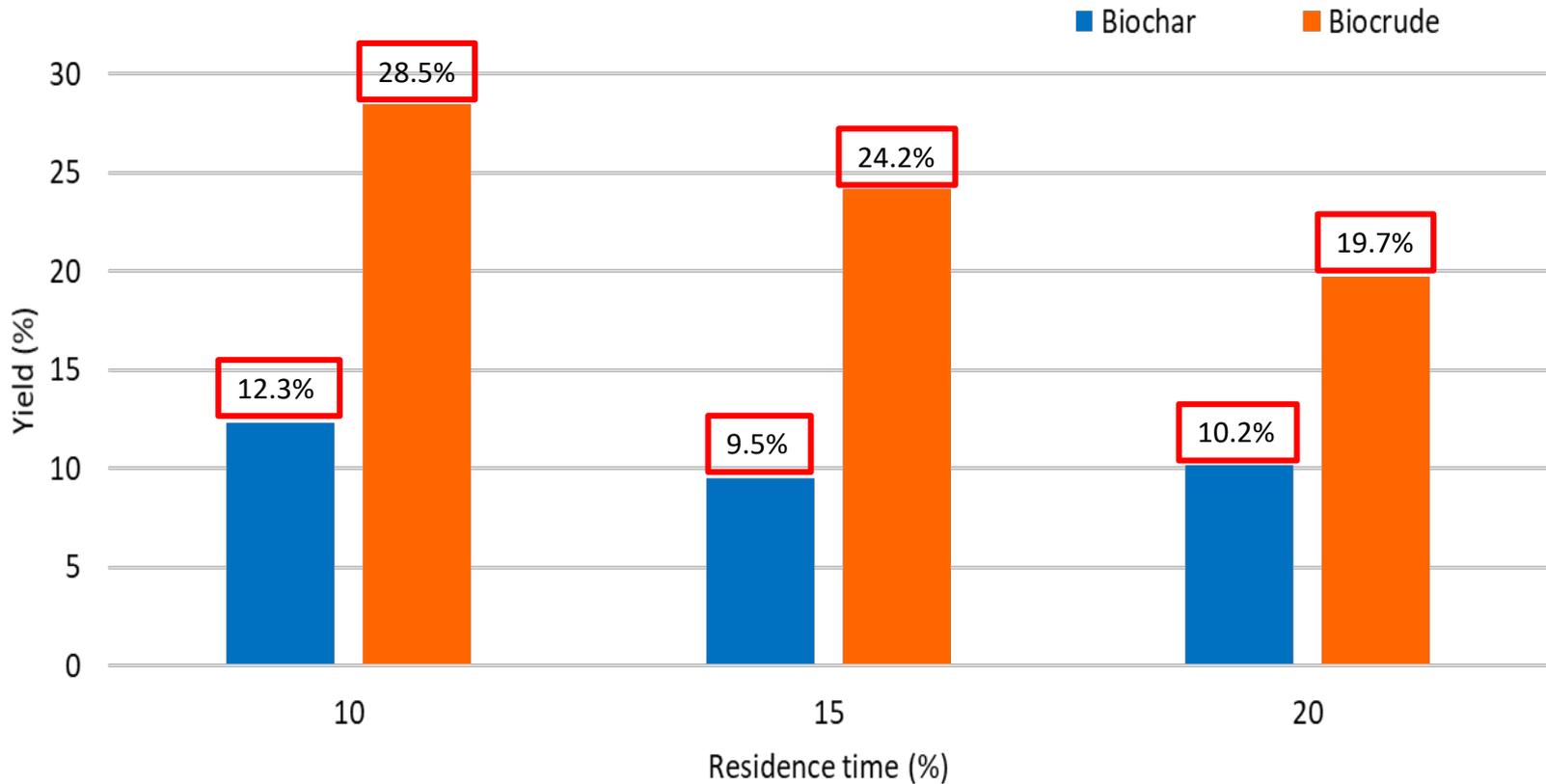


# Results: Temperature Profile



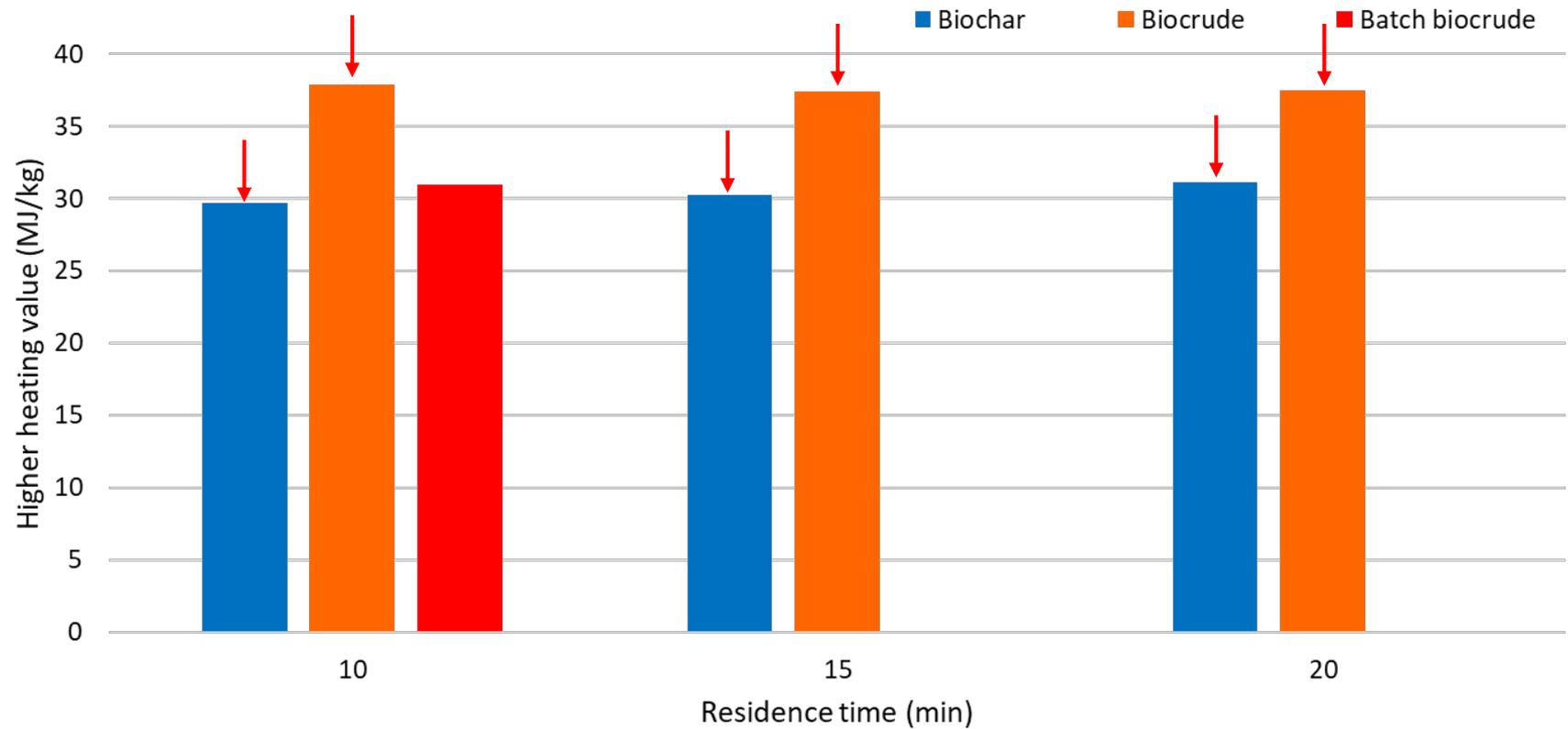


# Results: Yields





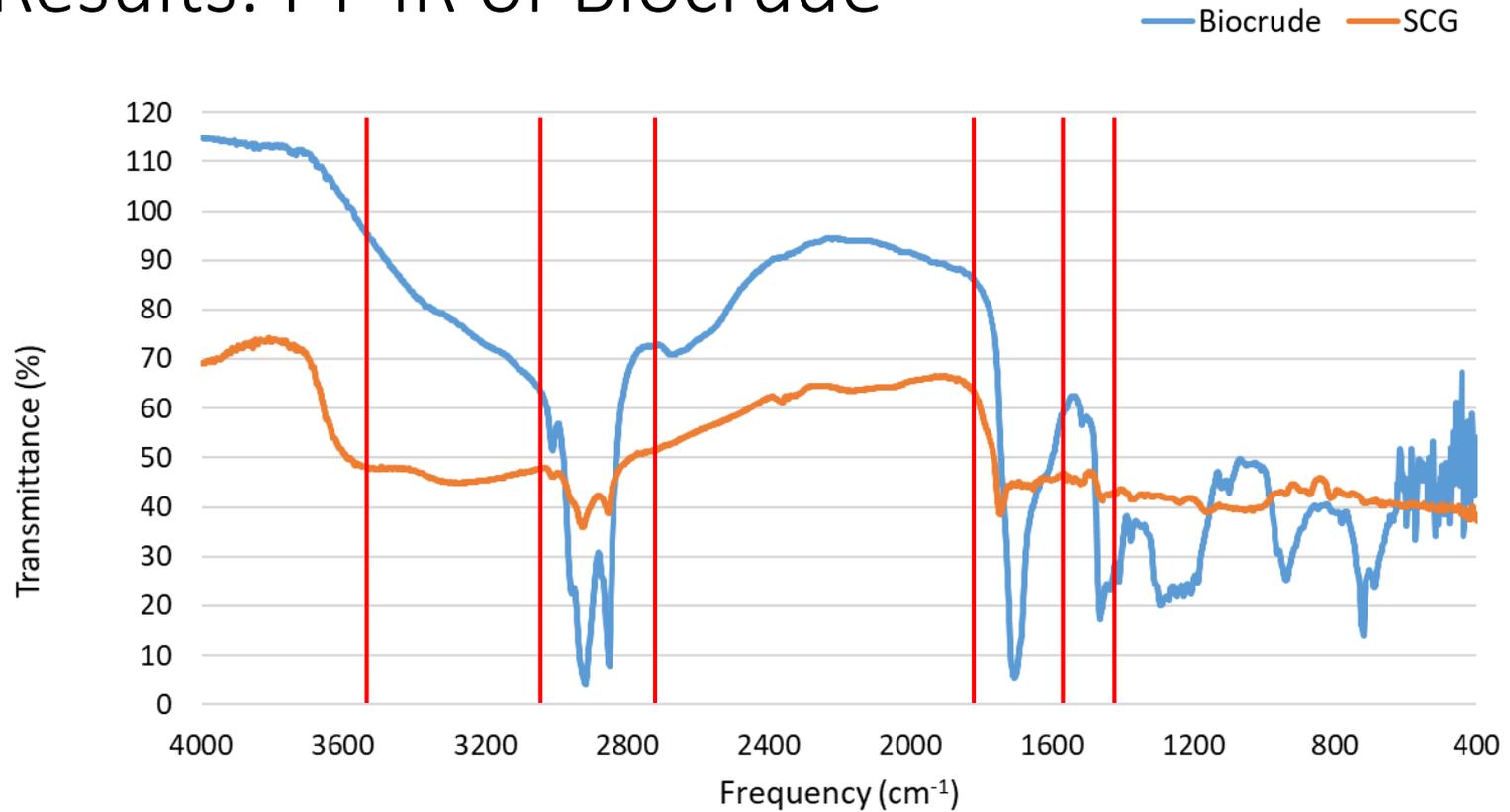
# Results: Higher heating value (HHV)



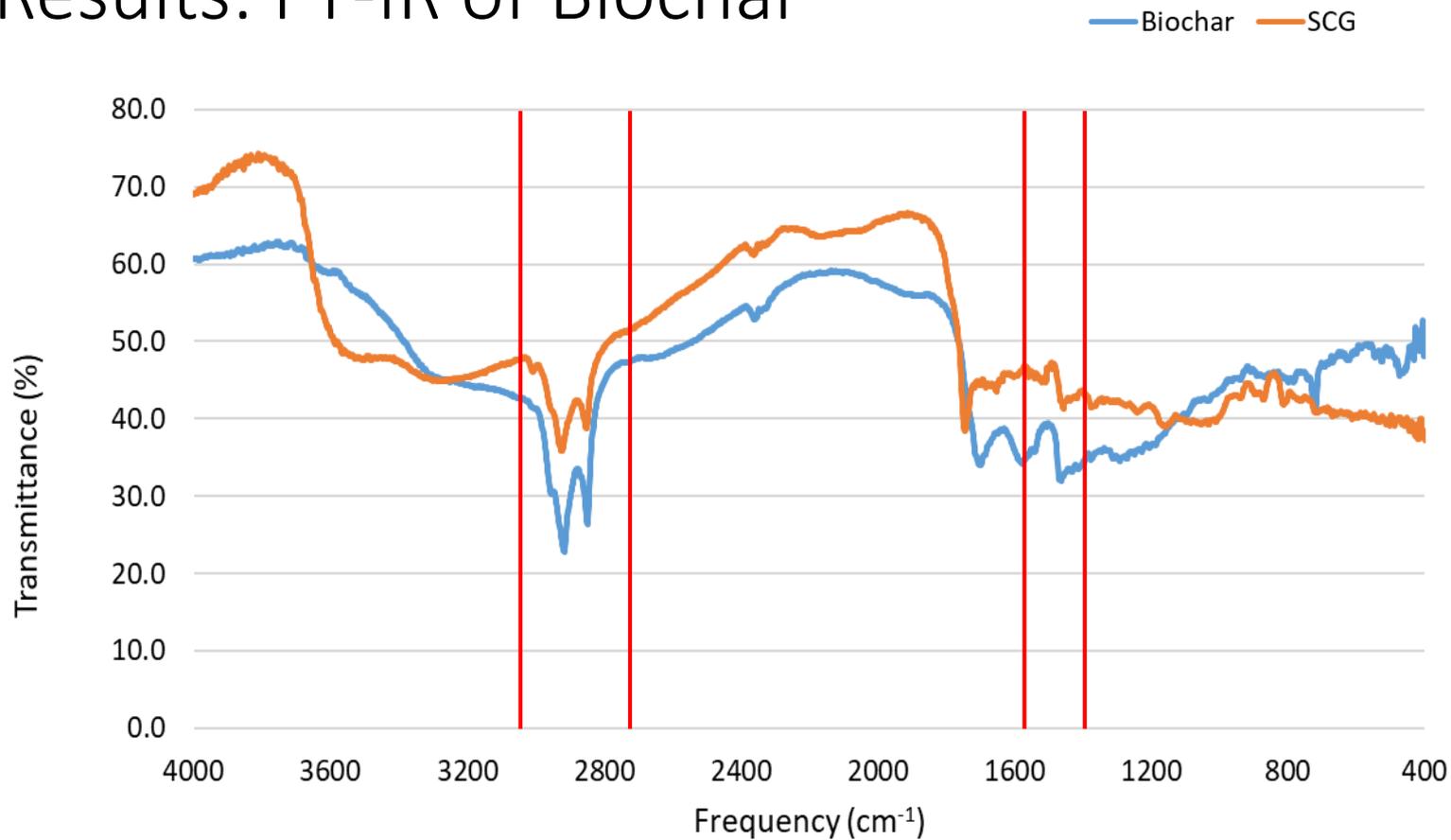
## Results: GC-MS

Component	Retention time (min)	Area (%)
Palmitic acid	32.769	34.46
Linoleic cid	35.643	29.92
Oleic acid	35.75	13.92
Stearic acid	36.161	9.67
Linoleic acid methyl ester	33.901	2.84
Methyl 9,12-Heptadecanoic acid	36.364	2.28

# Results: FT-IR of Biocrude



# Results: FT-IR of Biochar



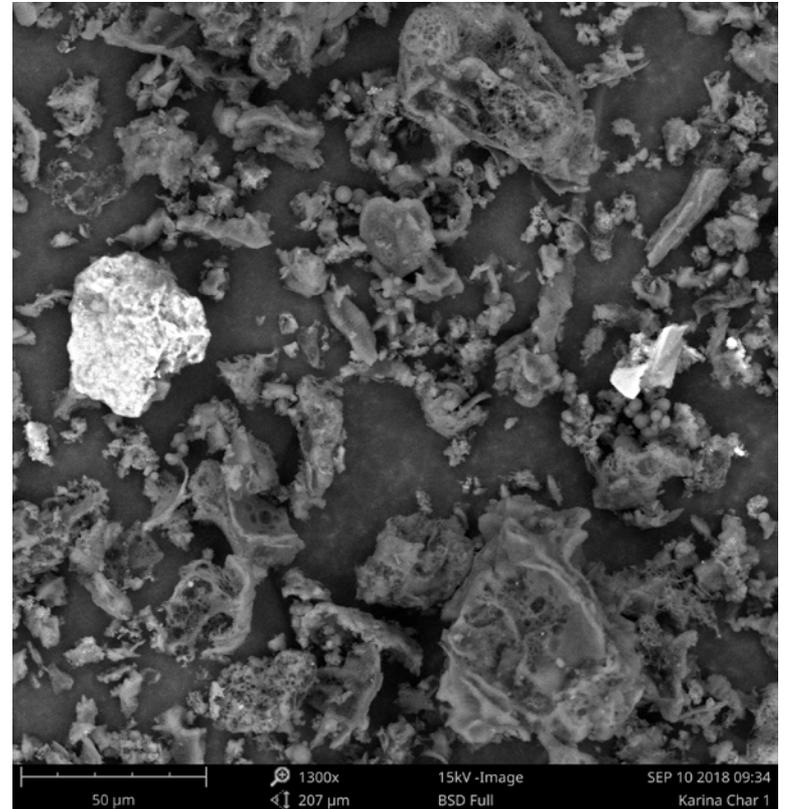
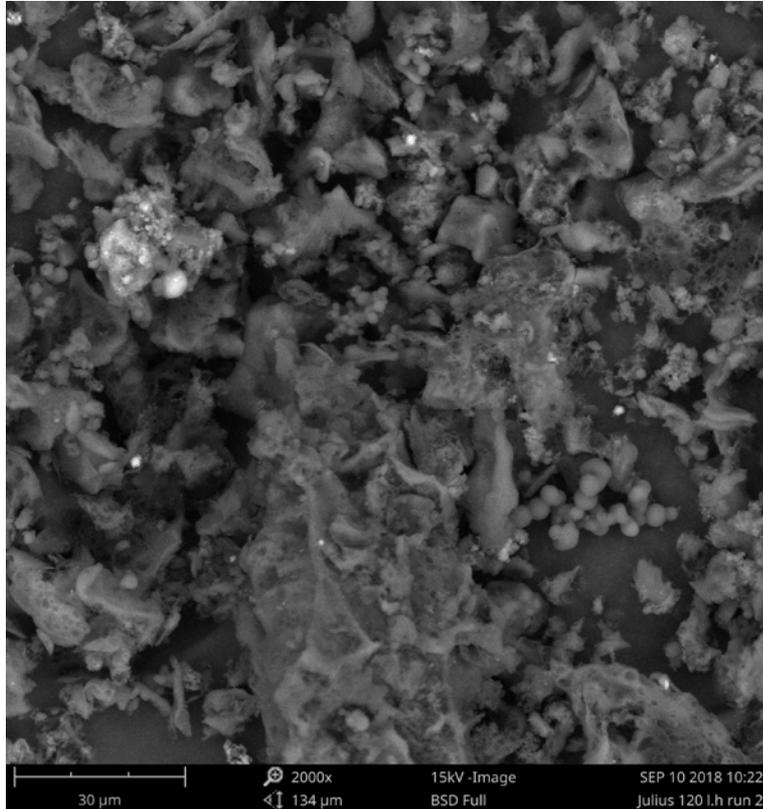
# Results: Proximate analysis of the biochar

Composition (%)				
Residence time(min)	Moisture	Volatiles	Fixed Carbon	Ash
10	1.7	44.6	50.3	3.7

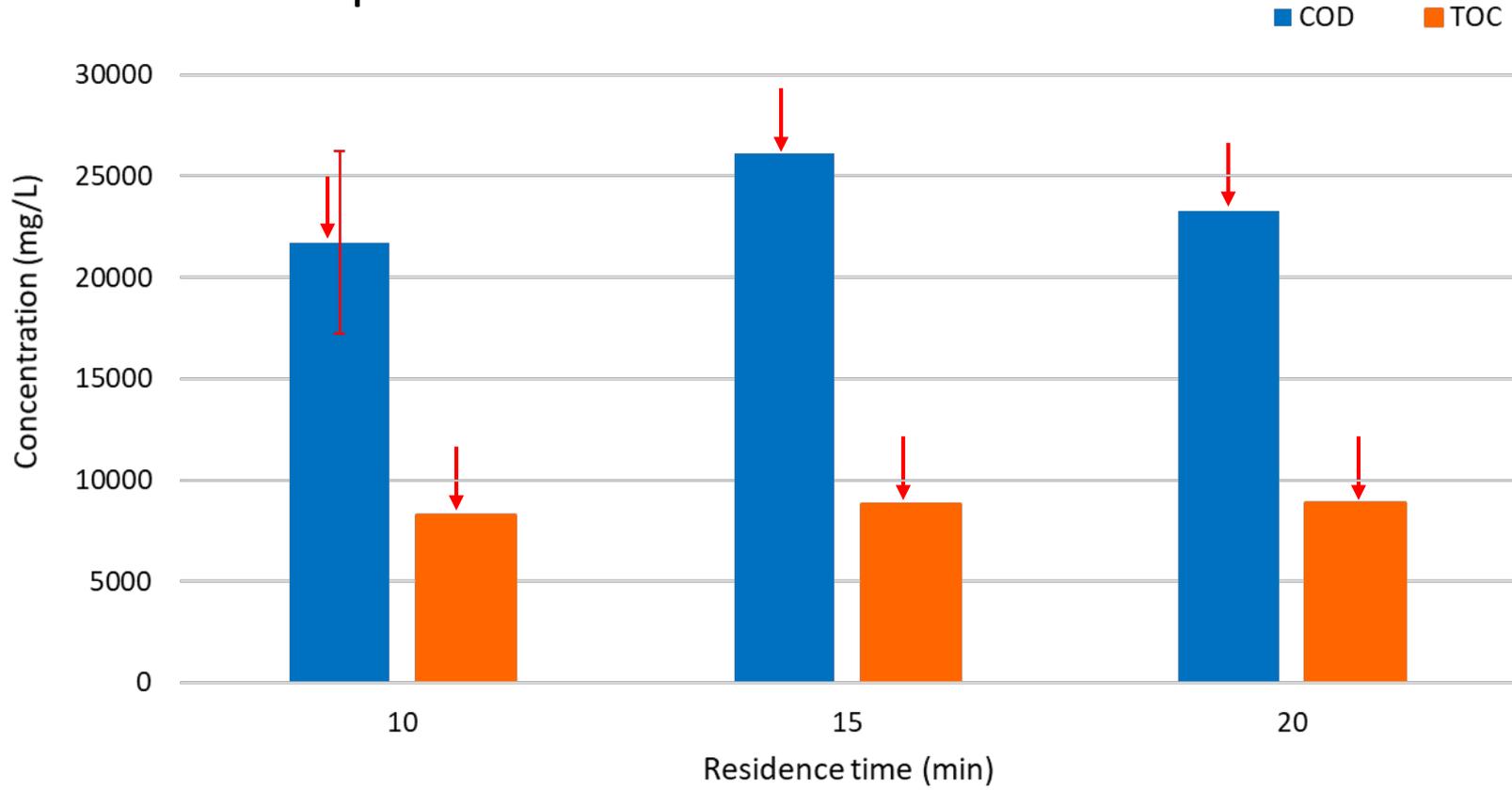
## Results: BET & BJH

Analysis	Result	
BET surface area	7.651	m <sup>2</sup> /g
Langmuir surface area	24.096	m <sup>2</sup> /g
BJH Adsorption cumulative surface area of pores	16.746	m <sup>2</sup> /g
BJH Desorption cumulative surface area of pores	19.751	m <sup>2</sup> /g
BJH Adsorption cumulative volume of pores	0.154	cm <sup>3</sup> /g
BJH Desorption cumulative volume of pores	0.155	cm <sup>3</sup> /g
Median pore width	13.280	nm

# Results: SEM of biochar



# Results: Aqueous Phase



## Conclusion:

- SCG produced high quality biochar and biocrude
- Residence time had a significant impact on the yields
- Residence time had no significant effect on the quality of the products

Thank you

# References

[1]Dell, R.M., and Rand, D.A.J.: 'Energy storage—a key technology for global energy sustainability', *Journal of Power Sources*, 2001, 100, (1), pp. 2-17

[2]Kondamudi, N., Mohapatra, S.K., and Misra, M.: 'Spent coffee grounds as a versatile source of green energy', *Journal of Agricultural and Food Chemistry*, 2008, 56, (24), pp. 11757-11760

[3]Yang, L., Nazari, L., Yuan, Z., Corscadden, K., and Xu, C.C.: 'Hydrothermal liquefaction of spent coffee grounds in water medium for bio-oil production', *Biomass and Bioenergy*, 2016, 86, pp. 191-198

[4]Manju, S., and Chadha, B.S.: 'Production of Hemicellulolytic Enzymes for Hydrolysis of Lignocellulosic Biomass-Chapter 9'

[5]Passos, C.P., and Coimbra, M.A.: 'Microwave superheated water extraction of polysaccharides from spent coffee grounds', *Carbohydrate polymers*, 2013, 94, (1), pp. 626-633